Amendments to the Claims:

This listing of claims will replace all prior versions, and listings, of claims in the application:

Listing of Claims:

- (Currently Amended) An apparatus for producing alcohol from plant cereal raw materials, comprising
 - a grinding station (1) which grinds to flour at least the grain comprising a starch and/or sugar of the cereal raw materials.
 - a liquefaction station (9) which digests flour to a liquiefied raw material,
 - a fermentation station (13) which ferments <u>said</u> liquefied raw material to mash.
 - a distillation station (15) separating off the alcohol from the mash, and
 - a drying station (21, 31) for <u>drying</u> vinasse arising in the distillation station
 (15),

characterized in that

for the production of alcohol-from cereals, a wherein the grinding station (1) which grinds to flour the grain comprising the starch and/or sugar of the cereals with the separation of separates at least a part of the seed coat portions enclosing the grain, and a liquefaction station (9) digesting the flour are provided and in that the separated seed coat portions which are separated off can be fed to the drying station (21, 31) as carrier medium for the vinasse drying, and wherein said drying station (21, 31) comprises a drier (21) which carries out the final drying of the vinasse produced as a residue in said distillation station (15) at

- a dew point temperature of above 95°C, and wherein the distillation station (15) comprises a distillation column (91) heated by the vapor of the drier (21).
- (Original) The apparatus as claimed in claim 1, characterized in that the grinding station (1) separates off the seed coat portions in a weight ratio of seed coat portions to flour of 1 to 9 to 2 to 8.
- (Previously Presented) The apparatus as claimed in claim 1, characterized in that the grinding station (1) grinds the cereals to flour with a mean particle size between 0.5 and 1 mm.
- (Previously Presented) The apparatus as claimed in claim 1, characterized in that the grinding station (1) has a roller mill or an impact jet mill.
- 5. (Currently Amended) The apparatus as claimed in claim 1, characterized in that, for producing alcohol from plant raw materials, in particular cereals ground to flour, a wherein said liquefaction station (9) digesting carbohydrates and/or sugars in the raw material is provided, which has a comprises at least one mixing stage comprising a mixing condenser (53) for admixing steam to the a product stream of the cemminuted ground cereal raw material or a suspension thereof, at least one mixing stage comprising mixing condenser (53), a steam-jet injector (57) downstream of the mixing condenser (9) and for admixing superheated steam to the product stream, and an expansion cooler (63) for the product

stream connected downstream of the steam-jet injector (57) and comprises at least one expansion stage (67, 73).

the <u>said</u> mixing condenser (53) admixing expansion vapor of the <u>said</u> expansion cooler (63) to the said product stream.

- (Currently Amended) The apparatus as claimed in claim 5, characterized in that
 <u>wherein</u> at least the <u>said</u> expansion cooler (63) is of multistage construction-and
 the mixing condenser (53) admixes to the product stream at least the expansion
 vapor of the first expansion stage (67) of the expansion cooler (67).
- (Original) The apparatus as claimed in claim 6, characterized in that the mixing condenser (53) is of single-stage construction, and the expansion cooler (63) is of two-stage construction.
- 8. (Previously Presented) The apparatus as claimed in claim 5, characterized in that the mixing condenser (53) heats the product stream to a temperature below the gelatinization temperature of the raw material, and the steam-jet injector (57) heats the product stream to a temperature above the gelatinization temperature of the raw material.
- (Previously Presented) The apparatus as claimed in claim 1, characterized in that, between the fermentation station (13) and the distillation station (15), there is disposed a degassing station (17) in which the mash product stream passes

through from top to bottom a vertically standing tube bundle (81) which is evacuated at its bottom end, and the mash product stream expands in the tube bundle (81).

- 10. (Original) The apparatus as claimed in claim 9, characterized in that the mash product stream, before entry into the tube bundle (81), passes through a heat exchanger (79) preheating the mash.
- 11. (Canceled).
- (Currently Amended) The apparatus as claimed in claim [[11]] 1, eharacterized in that the wherein said drier (21) produces essentially air-free exhaust vapor.
- (Currently Amended) The apparatus as claimed in claim [[11]] 1, eharacterized in that the wherein said drier (21) is constructed as a superheated steam drier.
- 14. (Previously Presented) The apparatus as claimed in claim 1, characterized in that the distillation station (15) has a first distillation column (91) which is heated, in particular, by exhaust vapor of the drying station (21, 31), to which is connected a dehydration station (45) which dehydrates its crude alcohol product stream

and in that a second distillation column (117) is connected at an intermediate level of the first distillation column (91) above its mash feed level (93), which

- second distillation column is heated via a heat exchanger (127) by heat of the dehydrated alcohol vapor of the dehydration station (45).
- 15. (Original) The apparatus as claimed in claim 14, characterized in that the heat exchanger is constructed as a falling-film evaporator (127) heated by dehydrated alcohol vapor of the dehydration station (45).
- (Previously Presented) The apparatus as claimed in claim 14, characterized in that the dehydration station (45) comprises a molecular sieve (117).
- (Original) The apparatus as claimed in claim 16, characterized in that the molecular sieve (117) is operated at a pressure of 1.7 bar absolute or more.
- 18. (Previously Presented) The apparatus as claimed in claim 1, characterized in that the drying station (21, 31) comprises a separator (25) which separates the vinasse into a vinasse-thin juice product stream and a vinasse-solids product stream, an evaporator (31) which evaporates the vinasse-thin juice product stream to form vinasse-thick juice, and also a drier (21) which dries the vinasse-thick juice together with the vinasse-solids to give dry vinasse, in that the distillation station (15) is connected downstream of the dehydration station (45) which dehydrates the crude alcohol product stream and in that the evaporator (31) has at least one evaporator stage (51) heated by heat of the dehydrated alcohol vapor of the dehydration station.

- (Original) The apparatus as claimed in claim 18, characterized in that the
 evaporator (31) comprises a pre-evaporator (49) and a final evaporator (51) and
 in that the final evaporator (51) is heated by dehydrated alcohol vapor from the
 dehydration station (45).
- (Previously Presented) The apparatus as claimed in claim 18, characterized in that the dehydration station (45) comprises a molecular sieve (117).
- (Original) The apparatus as claimed in claim 20, characterized in that the molecular sieve (117) is operated at a pressure of 1.7 bar absolute or more.
- (New) An apparatus for producing alcohol from a cereal grain raw material, comprising
 - grinding means for grinding said cereal grain raw material into a flour and separating at least a part of a seed coat portion enclosing said cereal grain raw material.
 - liquefying means for digesting said flour into a liquiefied raw material,
 - fermenting means for fermenting said liquefied raw material to form a mash.
 - distillation means comprising a distillation column for separating alcohol from said mash at a dew point temperature of above 95°C,
 - drying means comprising a drier for drying a vinasse formed as a residue

in said distillation means and for producing an exhaust vapor for heating said distillation column, and

 feeding means for feeding dry seed coat portions to said drying means as a carrier medium for said vinasse.